

In the Description

Please replace the paragraph commencing at page 9, line 18, with the following re-written paragraph.

--The silica and clay can be separated from the oil by filtration and/or centrifugation. The effective amount of silica gel is preferably from about 0.01% to 3% by weight of oil. The silica gel preferably includes TriSyl® S 627 silica gel or a Sorbsil® silica gel. --

Please replace the paragraph commencing at page 9, line 22, with the following re-written paragraph.

--In the process, the oil is preferably contacted with the silica for about 1 to 60 minutes. The effective amount of bleaching clay is preferably from about 0.1% to 3% by weight of oil. The clay can include Tonsil Supreme 120 FF bleaching clay, a Filtrol bleaching clay or a Pur-Flo® bleaching clay. The oil is preferably heated to about 75°C to 110°C after the oil contacts the bleaching clay. The oil preferably contacts the bleaching clay for about 5 to 30 minutes.--

Please replace the paragraph commencing at page 13, line 20, with the following re-written paragraph.

--The vacuum is then broken and nitrogen is bubbled through the oil and a silica, preferably a silica gel, is added. Silica gels that are available for use with oils are suitable. For example TriSyl® S 627, a silica gel ~~manufactured by~~ (W.R. Grace, of Baltimore, MD, USA) is a suitable and preferred material. Silica gels

are used in amounts of 0.01 % to 3 %, but more preferably in amounts of 0.1 % to 1 % and most preferably at 0.5 %. Other useful silicas include Sorbsil® silicas (Crosfield Company, Joliet, Illinois, USA).--

Please replace the paragraph commencing at page 13, line 30, with the following re-written paragraph.

--The vacuum is then again broken and replaced with a nitrogen atmosphere and 0.1 % to 3 %, more preferably 0.5 % to 2.0 % and most preferably 1.0 % of a bleaching clay commonly used for processing of oils is added. Tonsil Supreme 120 FF bleaching clay, which is manufactured by Quimica Sumex S.A. de C.V. of Mexico City, Mexico is a preferred clay, but other clays from the same manufacturer and clays from other manufacturers that are used for the purpose of processing oils may be used. For example, Filtrol bleaching clays (Engelhard Corp., Beachwood, Ohio, USA) and Pur-Flo® bleaching clays (Oil-Dri Corporation of America, Chicago, Illinois, USA) are useful.--

Please replace the paragraph commencing at page 15, line 8, with the following re-written paragraph.

--Vacuum on the reactor was then broken with nitrogen gas and 0.5 % TriSyl® S 627 silica gel was added to the oil. The reactor was then sealed again and evacuated. Temperature was maintained for 15 minutes of contact time of the silica/oil mixture. Vacuum was then broken with nitrogen gas, the reactor was opened, and 1 % Tonsil Supreme 120 FF bleaching earth was added to the silica/oil mixture. The reactor was closed again, evacuated and the silica/clay/oil

mixture was heated to 100°C and kept at that temperature for 15 minutes contact time.--

Please replace the paragraph commencing at page 25, line 10, with the following re-written paragraph.

--The silica/clay treatment was chosen to be the same, initially, as used in the other examples, but this was changed after the first 2,200 kg batch from 0.5 % TriSyl® 627 silica gel to 0.75%, and from 1 % Tonsil Supreme 124 FF bleaching clay to 1.5 % to try to improve pretreated oil colour, which was judged to be darker than desirable with the first batch processed.--

Please replace the paragraph commencing at page 26, line 14, with the following re-written paragraph.

--The silica/clay treated oil was of good quality, except that the colour of the first batch was 0.7 R, which was higher than experienced in the previous examples. With all subsequent pretreatment batches (8 out of a total of 9) Trisyl® silica gel was increased from 0.5 % to 0.75 % and Tonsil bleaching clay from 1 % to 1.5 %. This reduced colour by 0.2 R/5 Y to 0.5 R/8 Y similar to previous results. PV's and AV's were satisfactory. --